

DATA REPOSITORY ITEM 2009118

THERMODYNAMIC MODELLING

Abiogenic endmember compositions for Nisyros have been computed from equation (4) considering the following temperature dependencies for $f_{\text{H}_2\text{O}}$ of 2 m NaCl solutions and K_3 , respectively:

$$\log f_{\text{H}_2\text{O}} = 5.462 - 2047/T \quad (\text{S1})$$

$$\log K_3 = 10.5 - (5150 + 310 \cdot n)/T \quad (\text{S2})$$

where T is in K and n the number of carbon atoms in ethane and propane, respectively (Chiodini et al., 2001; Taran and Giggenbach, 2003).

Carbon isotope data for CH_4 and CO_2 reflect hydrocarbon formation temperatures of $340 \pm 10^\circ\text{C}$ (Table 1). At these temperatures, the redox conditions of the bi-phase hydrothermal system can be constrained considering gas concentration data of the fumaroles. For the period from 1990-2002, molar ratios (X) of redox pairs CO/CO_2 , $\text{H}_2/\text{H}_2\text{O}$ and CH_4/CO_2 indicate that redox conditions at 340°C closely correspond to the $\text{FeO}-\text{FeO}_{1.5}$ buffer (Chiodini and Marini, 1998; Marini and Fiebig, 2005), for which $\log(X_{\text{H}_2}/X_{\text{H}_2\text{O}})$ is -2.82 , roughly independent of temperature (Giggenbach, 1987). $X_{\text{CO}}/X_{\text{CO}_2}$ and $X_{\text{CH}_4}/X_{\text{CO}_2}$ ratios were also measured for the fumaroles sampled in this study and are indistinguishable from values observed for the period 1990-2002 (Table 1S). This agreement indicates that no significant change in redox conditions took place between 1990 and 2007. The f_{CO_2} at the temperature of methane formation can be constrained from molar ratios of CO and H_2 using equation S3 (Chiodini & Marini, 1998), along with gas concentration data and methane formation temperatures reported by Fiebig et al. (2007):

$$\log f_{\text{CO}_2} = -2.485 + 2248/T - \log(X_{\text{H}_2}/X_{\text{CO}}) + \log f_{\text{H}_2\text{O}}$$

(S3)

At Nisyros, f_{CO_2} is $\sim 1\text{bar}$ (Table 1S), such that $\log f_{\text{CO}_2}$ in equation (4) can be neglected.

MIXING TRENDS DISPLAYED IN FIGURE 1

Hydrocarbon distribution ratios of C1/C2 and C2/C3 are given through

$$C_i/C_{i+1} = (nC_{i,\text{ab}} + nC_{i,\alpha}) / (nC_{i+1,\text{ab}} + nC_{i+1,\alpha}) \quad (\text{S4})$$

with nC_{ab} and nC_{α} denoting the moles of alkane hydrocarbons with carbon numbers i and $i+1$, predicted by thermodynamics according to equation (4) (ab) and by random breakage or linkage of C-bonds (α), respectively. The Schulz-Flory distribution factor α is defined by

$$\alpha = nC_{i+1,\alpha} / nC_{i,\alpha} \quad (\text{S5})$$

The mole fraction of abiogenic equilibrium alkanes with C-numbers i and $i+1$ is represented by Y according to

$$Y_{i+1/i} = nC_{i+1,\text{ab}} / nC_{i,\text{ab}}$$

$$(\text{S6})$$

Values for Y can be computed from equation (4). If reaction (5) applies for abiogenic hydrocarbon production, only methane is generated and Y becomes 0. For a given chain length, molar fractions of hydrocarbons generated through random breakage or linkage (X_{α}) or through abiogenic processes (X_{a}) are interlinked through

$$X_{\text{b}} = 1 - X_{\alpha} = nC_{\text{a}} / nC = (1 - nC_{\alpha} / nC) \quad (\text{S7})$$

Considering equation (S4) to (S7), it can be derived for C1/C2 and C2/C3 ratios

$$C1/C2 = 1 / ((1 - X_{\alpha}) * Y_{2/1} + \alpha * X_{\alpha}) \quad (\text{S8})$$

$$C2/C3 = ((1 - X_{\alpha}) * Y_{2/1} + \alpha * X_{\alpha}) / ((1 - X_{\alpha}) * Y_{2/1} * Y_{3/2} + \alpha * \alpha * X_{\alpha}) \quad (\text{S9})$$

46

TABLE

Table DR1. Molar ratios, X , of gas components contained in dry gas samples and comparison of $X_{\text{CH}_4}/X_{\text{CO}_2}$ and $X_{\text{CO}}/X_{\text{CO}_2}$ ratios obtained in 2007 with those characteristic for the 12 year period (1990-2002; Marini & Fiebig, 2005). Also given are $\log f_{\text{CO}_2}$ values characteristic for

the Nisyros bi-phase hydrothermal system, which were calculated according to equation S3 and temperatures derived from carbon isotope partitioning between CO₂ and CH₄ (see Table 1).

REFERENCES CITED

- Chiodini, G., and Marini, L., 1998, Hydrothermal gas equilibria: The H₂O-H₂-CO₂-CO-CH₄ system: *Geochimica et Cosmochimica Acta*, v. 62, p. 2673-2687.
- Chiodini, G., Marini, L., and Russo, M., 2001, Geochemical evidence for the existence of high-temperature hydrothermal brines at Vesuvius volcano, Italy: *Geochimica et Cosmochimica Acta*, v. 65, p. 2129-2147.
- Fiebig, J., Woodland, A.B., Spangenberg, J., and Oschmann, W., 2007, Natural evidence for rapid abiogenic hydrothermal generation of CH₄: *Geochimica et Cosmochimica Acta*, v. 71, p. 3028-3039.
- Giggenbach, W.F., 1987, Redox processes governing the chemistry of fumarolic gas discharges from White Island, New Zealand: *Applied Geochemistry*, v. 2, p. 143-161.
- Marini, L., and Fiebig, J., 2005, Fluid geochemistry of the magmatic-hydrothermal system of Nisyros (Aegean arc, Greece), in Hunziker, J.C., and Marini, L., eds., *The geology, geochemistry and evolution of Nisyros volcano (Greece); implications for the volcanic hazards: Memoires de Geologie (Lausanne)*, v. 44, p. 121-163.
- Taran, Y.A., and Giggenbach, W.F., 2003, Geochemistry of light hydrocarbons in subduction-related volcanic and hydrothermal fluids: *Society of Economic Geologists, special Publication*, v. 10, p. 61-74.

Sample	X(CO₂)	X(CH₄)	X(CO)	X(H₂)	log(CO/CO₂)	log(CO/CO₂)_{12yr}	log(CH₄/CO₂)	log(CH₄/CO₂)_{12yr}	logf(CO₂)
Polybotes Mikros (PP9S)	743300	1759	9.0	16000	-4.9	-4.8 to -5.5	-2.6	-2.5 to -3.0	0.0
Stefanos (S4)	791500	4400	2.2	6200	-5.6	-5.4 to -6.1	-2.3	-2.1 to -2.6	-0.1
Phlegeton (A)	809300	805	2.1	9230	-5.6	-5.3 to -6.0	-3.0	-2.4 to -3.2	-0.3